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A METHOD PERTAINING TO COMBUSTION, AND A BURNER

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The present invention relates to a method pertaining to combustion, and to a burner. More specifically, the invention relates to a method and to a burner for the combustion of oxygen gas in respect of heating furnaces.

When combusting hydrocarbons in combination with high oxygen concentration, flame temperatures in excess of 2000 degrees C are normally reached, together with furnace atmospheres of very high partial pressures of carbon dioxide and steam. This results in drawbacks, such as high NO<sub>x</sub>-contents and local overheating problems.

It is highly desirable to design burners that have emission diminishing properties.

The present invention satisfies this desideratum.

Accordingly, the present invention relates to a method pertaining to the combustion of a fuel with an oxidant in a heating furnace, where the fuel and the oxidant are delivered to a burner head, and is characterized in that in a first method step fuel and oxydant are caused to be emitted from the burner head in the close proximity of one another so that the process of combustion will take place essentially close to and at a small distance out from the burner head until there is reached in the furnace space a temperature that exceeds the spontaneous combustion temperature of the fuel and in that in a second method step the fuel and the oxidant are then caused instead to be emitted from the burner head in mutually spaced relationship so that the process of combustion will take place essentially at a distance from the burner head corresponding to at least the diameter of the burner head and out from the burner.

The invention also relates to a burner of the kind and with the general features set forth in claim 9.

The invention will now be described in more detail, partly with reference to exemplifying embodiments of the invention illustrated in the accompanying drawings, in which

- Fig. 1 is a straight-on front view of a burner head according to a first embodiment;
- Fig. 2 is a straight-on view of a burner head according to a second embodiment;

- Fig. 3 is a diagrammatic illustration of a burner head and a flame as seen from one side when the burner is operated in a first manner; and
- Fig. 4 is a diagrammatic illustration of a burner head and a flame as seen from one side when the burner is operated in a second manner.

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The inventive method thus pertains to the combustion of a fuel with an oxidant in a heating furnace, in which the fuel and the oxidant are delivered to a burner head. The burner head is mounted in a known manner in a furnace wall, so that the flame produced in the combustion process will extend into the furnace chamber.

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The invention is characterized in that the combustion process takes place in two steps, where the second step affords advantages over the known technology.

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In a first method step, fuel and oxidant are emitted from the burner head in close relationship with one another, so that the process of combustion will essentially take place close to and slightly spaced from the burner head. This method is known per se, in which the burner is designated "Oxy-fuel"-burner.

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In this first step of the method, the burner is operated until a temperature exceeding the spontaneous combustion temperature of the fuel is reached in the furnace chamber.

The second step of the combustion process may conveniently be initiated when the furnace temperature is above roughly 750 degrees C.

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According to the invention, this second method step is carried out when this temperature or a still higher temperature has been reached. In this second method step, the fuel and the oxidant are caused instead to be emitted from the burner head at a distance from each other, so that combustion will take place generally at a distance from the burner head that corresponds at least to the diameter of the burner head and out from the burner.

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It is preferred that in the first method step the fuel is caused to be emitted from a nozzle 2 in the burner head 1 and the oxidant is caused to be emitted from outlet openings 3 placed concentrically around the nozzle 2; see figure 1.

It is also preferred that in the second method step, the fuel is caused to be emitted from a nozzle 2 in a burner head 1 and that the oxidant is emitted from outlet openings 4,5 located on one side of and at a distance from said nozzle 2; see figure 1.

- 5 According to one preferred embodiment of the invention, the outlet openings 4, 5 are comprised of Laval nozzles or venturi-nozzles.

The opening 6 functions to monitor the flame.

- 10 According to one preferred embodiment of the invention, the outlet openings 4, 5 are spaced from the fuel nozzle 2 by a distance that exceeds half the diameter of the burner head.

It has been found that a distance of about 40 mm suffices to afford the desired effect.

- 15 The burner thus permits two different *modus operandi*, partly as a typical oxy-fuel burner and partly as a burner which functions to produce a flame of essentially lower maximum temperature. This lower flame temperature is adapted to lie beneath the temperature at which the formation of NO<sub>x</sub> is limited by the reaction kinetics, this temperature being about 1550 degrees C.

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This is achieved by the aforesaid placement of the oxygen outlet openings 4, 5 and the fuel nozzle, whereby fuel and oxygen are combusted further away from the burner head in comparison with a conventional oxy-fuel-combustion process. This is illustrated in figures 3 and 4, where figure 3 illustrates the mutual relationship between the length and the propagation of the flames 7, 8 in the respect of oxy-fuel-combustion, and figure 4 illustrates the mutual relationship between the length and the propagation of said flames in the case of combustion according to the second step of the inventive method.

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- 30 The concept of the invention resides in lowering the oxygen content in the combustion zone, despite the oxidant having an oxygen content of more than 80%, by virtue of separation, high pressure and an optimized nozzle placement. This is achieved with a nozzle configuration that affords a high subpressure on those surfaces of the nozzle that lack medium-emitting nozzles. As a result of the subpressure, flue gases are sucked in from the furnace atmosphere and quickly mix with the out flowing media and therewith create turbulence. The mixing medium,

i.e. the furnace atmosphere, typically has an oxygen content of 0.5-10%. The remainder of the gas is comprised of  $\text{CO}_2$  and  $\text{H}_2\text{O}$  and  $\text{N}_2$  in varying mixtures.

5 Because  $\text{CO}_2$ ,  $\text{H}_2\text{O}$  and  $\text{N}_2$  do not actively take part in the combustion process, these constituents act as "combustion retardants". The dilution of the oxygen and the fuel is very high. Typically, oxygen concentrations of 7-15 % are reached in the combustion process, despite the use of pure oxygen. When applying the present invention there is obtained at process temperatures above said spontaneous combustion temperature a diffused but controlled combustion that significantly lowers the formation  $\text{NO}_x$  gases, primarily  $\text{NO}$  and  $\text{NO}_2$ .

10 As a result, fuel and oxidant will be mixed with the furnace flue gases before the fuel and oxydant gases meet one another. This gives a larger and colder flame 8 in spite of the efficacy corresponding to that achieved when combustion is effected according to known technology.

15 The nozzles can be directed conveniently straight forward, i.e. they need not be directed away from or towards each other, although they may be angled towards or away from the longitudinal axis of the burner head.

20 According to one preferred embodiment of the inventive method, the oxydant is gaseous and is given an oxygen concentration of 85 % or higher.

25 According to one significant feature of the inventive method, the oxidant is delivered to the burner at a pressure of at least 2 bar overpressure. Because the flame temperature is lower and the mixture of gas in the furnace volume is greater than in the case of oxy-fuel-combustion, the formation of  $\text{NO}_x$  is minimized while the temperature differences in the furnace space are dramatically lowered at the same time.

30 In comparison with conventional combustion devices used in industrial processes, application of the inventive method results in a lowering of  $\text{NO}_x$  formations by more than 90 %, without impairing the efficiency of the process and without the supply of substances other than those required for the combustion.

A burner nozzle according to the present invention is no larger than a known burner head for oxy-fuel-combustion. In a preferred embodiment of the invention, the burner nozzle has a diameter of about 70mm.

- 5 The compact method enables the invention to be applied in equipment already possessed by the user. Moreover, the equipment can be placed in a small water-cooled protective casing for application at very high process temperatures.

10 The aforesaid advantages are achieved in accordance with the invention with a selected fuel, solid fuel, gaseous fuel or liquid fuel. The inventive arrangement can replace existing combustion systems in principal without re-constructing the furnace equipment used for the process.

It is beneficial when the fuel used is oil, propane or natural gas.

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The burner head shown in figure 1 is intended for oil as fuel.

Figure 2 shows a burner head 10 for natural gas as fuel. The nozzle 11 is intended for natural gas. The outlet openings 12, 13, 14 are intended for the oxidant. The opening 15 is intended for monitoring the flame and the opening 16 is intended for a pilot flame.

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Because oxidant and the fuel nozzles can be directed straight forwards, there is obtained a construction that is inexpensive, easy to maintain and can be applied in existing processes without requiring measures other than the exchange of the nozzle construction.

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The oxidant is injected into the combustion space via one or more nozzles in the form of Laval nozzles or venturi nozzles. The oxidant will preferably be under an overpressure of at least 2 bar. The higher the pressure, the better the efficacy of the invention. A preferred pressure for normal applications is 4-5 bar. The fuel is injected via conventional nozzles at the pressure available.

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Although the invention has been described above with reference to a number of exemplifying embodiments it will be understood that the design of the burner head can be varied. For

instance, the burner head may include more oxidant outlet openings than those shown. Moreover, the placement of the fuel nozzle may be different to that shown in the drawings.

It will therefore be understood that the present invention is not restricted to the embodiments  
5 described above, but can be varied within the scope of the accompanying claims.